
Transport, mixing and agglomeration of particles in turbulent flows



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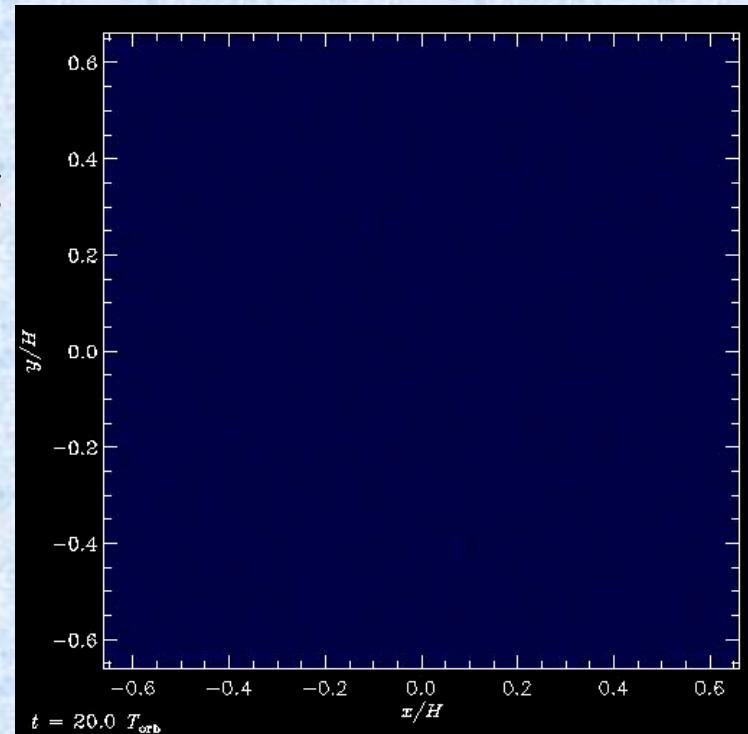
Gas - particle / droplet flows

Dilute flows

- Pollutant dispersion : PM10s
- Aerosol formation
 - Smoke - radioactive releases
- Weather - rain, mist and fog

Dense flows

- Volcanic eruptions
- Fluidized beds
- Mixing & combustion
- Pneumatic conveying
- Fouling / deposition
- Spraying
- Planet formation from inter-stellar dust



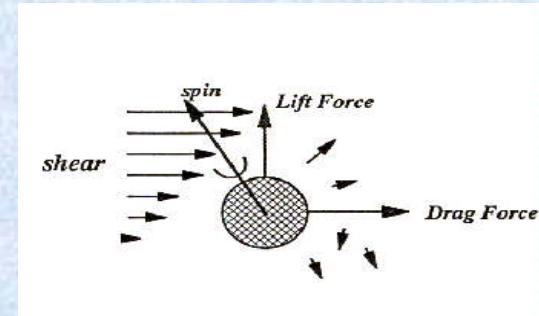
Outline

- Background
 - Scope of the physics in gas particle droplet flows
 - Role of inertia / Stokes number
- One-particle transport/dispersion
 - PDF approach
 - Dispersion in simple / complex flows
 - Transport in a turbulent boundary layer
 - Deposition and concentration
- Two-particle transport
 - Methods and approaches
 - Segregation
 - collisions

Gas-droplet / particle flows: scope of the physics

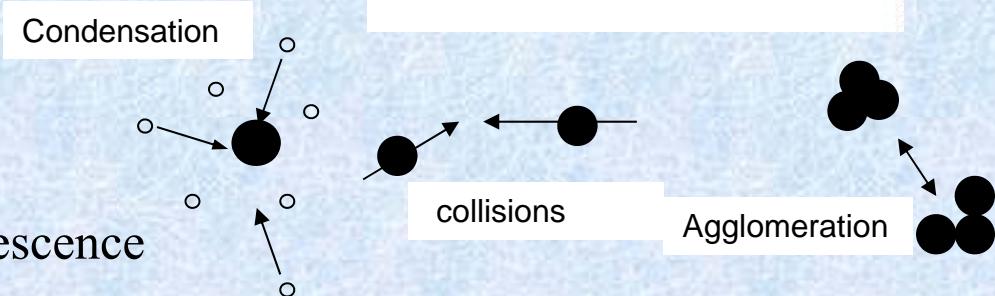
- Transport / dispersion

- Equation of motion
 - Aerodynamic forces
 - Stokes number $St = \tau_p / \tau_f$



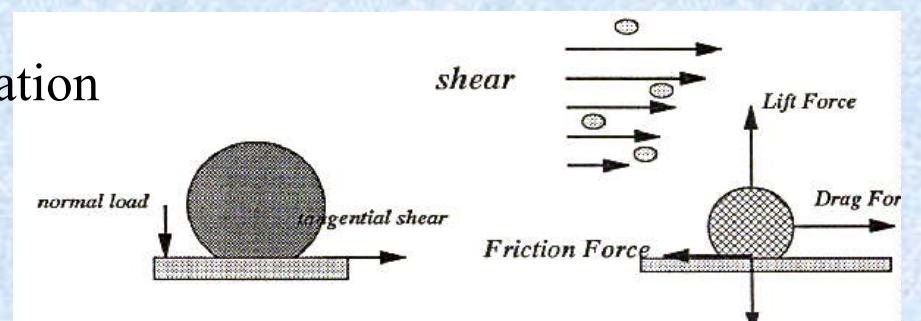
- Formation and growth

- Condensation / evaporation
 - Collisions / agglomeration/coalescence



- Two way coupling

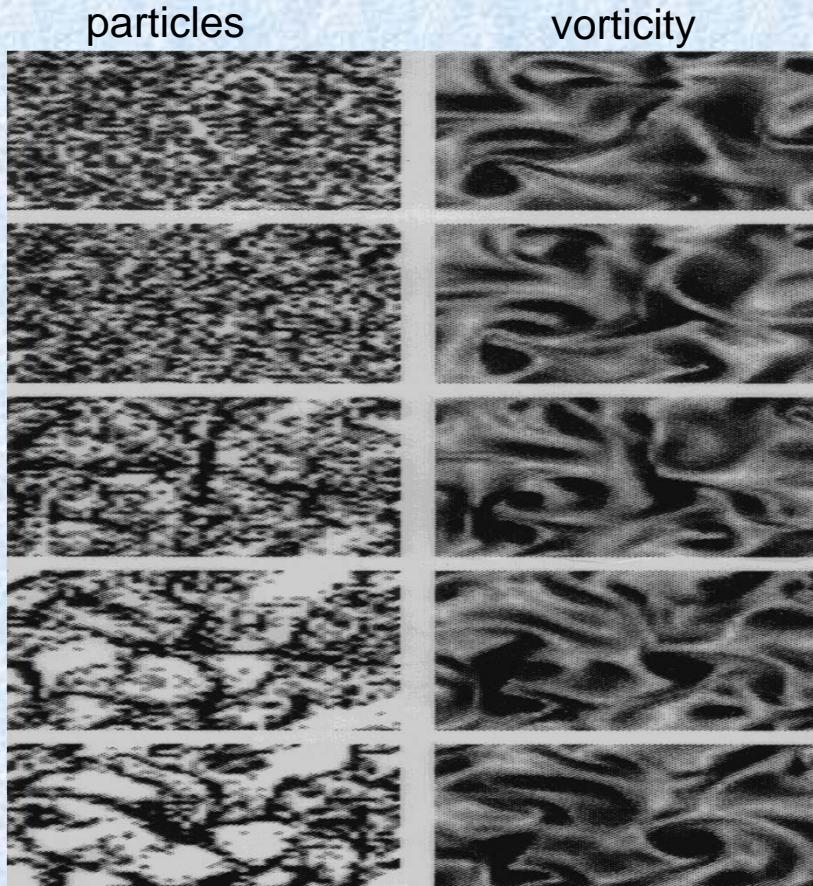
- interfacial drag/turbulence modification



- Boundary conditions

- Bounce / resuspension

Unmixing by turbulent flows



Wang & Maxey JFM 1993

Symposium Particle Transport, University of Aarhus 6-7 Nov, 2014



Need for a PDF approach

- Two-fluid approach
 - Representing the dispersed phase as a fluid in same way as carrier flow
 - What are the continuum equations-constitutive relations?
 - Does it behave as a simple Newtonian fluid?
 - Boundary conditions (near wall behaviour)
 - Particle segregation
 - Interaction with turbulent structures
 - Pair dispersion
 - Collision processes
 - Need for a statistical approach c.f. Kinetic theory of gases
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Slide 6

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Administrator; 24-06-2010

PDF Transport Equations

phase space vector

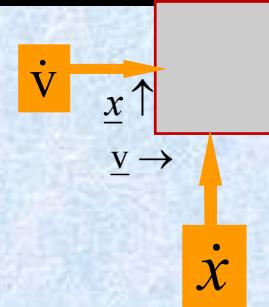
$$\underline{X} = (\underline{x}, \underline{v}, m, T)$$

phase space density

$$W(\underline{X}, t)$$

mass conservation

$$\frac{\partial W}{\partial t} + \frac{\partial}{\partial \underline{X}} \cdot (\dot{\underline{X}} W) = 0$$



$\Delta v \Delta x$
phase space vol

Eqns of Motion : $\dot{\underline{x}} = \underline{v}$; $\dot{\underline{v}} = \beta(\underline{u} - \underline{v})$; $\dot{m} = f\left(\frac{\alpha_v}{\alpha_{sv}}\right) Sh(\text{Re}_p, Sc)$; $\dot{T} = \dot{T}(\text{Re}_p, \text{Pr})$

$$F_a = \frac{1}{2} \rho_f C_D(\text{Re}_p) |\underline{u} - \underline{v}| (\underline{u} - \underline{v}),$$

$\beta^{-1} = \tau_p(|\underline{u} - \underline{v}|, \text{Re}_p)$ - particle relaxation time

$$P = \langle W \rangle; \dot{\underline{X}} = \langle \dot{\underline{X}} \rangle + \underline{X}'$$

Averaged (PDF) Eqn;

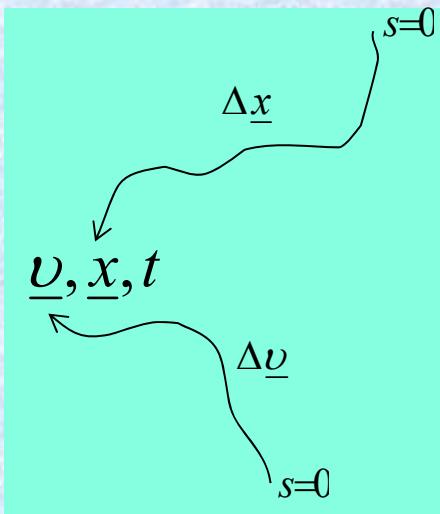
$$\frac{\partial P}{\partial t} + \frac{\partial}{\partial \underline{X}} \cdot (\langle \dot{\underline{X}} \rangle P) = - \frac{\partial}{\partial \underline{X}} \cdot (\langle \dot{\underline{X}}' W \rangle) + \left(\frac{\partial P}{\partial t} \right)_{coll} d_p^2 \iint \Delta p_2(v_1, x, x + d_p \hat{k}, t) v_{21} \cdot \hat{k} dk dv_2$$

Simonin Zaichik

Gas-particle flow $\frac{\partial P}{\partial t} + \frac{\partial}{\partial \underline{x}} \cdot \underline{v} P + \frac{\partial}{\partial \underline{v}} \cdot \beta(\langle \underline{u} \rangle - \underline{v}) P = - \frac{\partial}{\partial \underline{v}} \cdot \boxed{\beta \langle \underline{u}' W \rangle}$ net force due to turbulence

Closure approximations for $\langle \beta \underline{u}' W \rangle$

$$\langle \beta \underline{u}'(\underline{x}, t) W(\underline{v}, \underline{x}, t) \rangle = - \left(\frac{\partial}{\partial \underline{v}} \cdot \underline{\mu} + \frac{\partial}{\partial \underline{x}} \cdot \underline{\lambda} + \underline{\kappa} \right) \langle W \rangle$$



$$\begin{aligned} \underline{\mu} &= \overbrace{\beta \langle \Delta \underline{v}(\underline{v}, \underline{x}, t | 0) \underline{u}'(\underline{x}, t) \rangle}^{\text{diffusion in velocity}} & \underline{\lambda} &= \overbrace{\beta \langle \Delta \underline{x}(\underline{v}, \underline{x}, t | 0) \underline{u}(\underline{x}, t) \rangle}^{\text{diffusion in x-space}} \\ \underline{\kappa} &= - \underbrace{\left\langle \Delta \underline{x}(\underline{v}, \underline{x}, t | 0) \cdot \frac{\partial}{\partial \underline{x}} \underline{u}'(\underline{x}, t) \right\rangle}_{\text{body force}} & \text{LHDI Approximation} \\ &&& \text{Reeks,} \end{aligned}$$

$$\begin{pmatrix} \mu \\ \lambda \end{pmatrix} = \beta \int_0^t \begin{pmatrix} \dot{g}(t-s) \\ g(t-s) \end{pmatrix} \left\langle \left\langle \underline{u}'(\underline{x}_p(s), s) \underline{u}'(\underline{x}, t) \right\rangle_{\underline{x}_p} \right\rangle ds$$

Furutsu Novikov

Zaichek, Swailes, Minier

Moments of PDF Eqns

spatial density $\langle \rho \rangle = \int d\underline{v} P(\underline{v}, \underline{x}, t)$; mean velocity $\bar{\underline{v}} = \langle \rho \rangle^{-1} \int d\underline{v} P(\underline{v}, \underline{x}, t) \underline{v}$;

Velocity fluctuations $\underline{v}' = \underline{v} - \bar{\underline{v}}$ $\overline{v'_i{}^l v'_m{}^m v'_n{}^n} = \langle \rho \rangle^{-1} \int d\underline{v} P(\underline{v}, \underline{x}, t) v'_i{}^l v'_m{}^m v'_n{}^n$

mass

$$\frac{\partial \langle \rho \rangle}{\partial t} + \frac{\partial}{\partial \underline{x}} \cdot \langle \rho \rangle \bar{\underline{v}} = 0$$

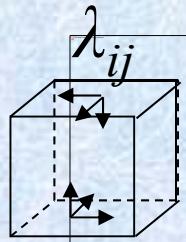
momentum

$$\langle \rho \rangle \frac{D}{Dt} \bar{v}_i = - \frac{\partial}{\partial x_j} \langle \rho \rangle \overline{v'_i v'_j} + \beta (\langle u_i \rangle - \bar{v}_i) \langle \rho \rangle + \beta \langle \rho \rangle \bar{u'_i}$$

Reynolds /kinetic stresses

Net force due turbulence

Momentum Eqn from PDF Eqn.



pressure tensor

$$\beta \langle \rho \rangle \bar{u}'_i = - \frac{\partial}{\partial \underline{x}} \cdot \underline{\lambda} \langle \rho \rangle + \underline{\kappa} \langle \rho \rangle$$

net turbulent driving force

body force

$$\langle \rho \rangle \frac{D \bar{v}_i}{Dt} = - \frac{\partial}{\partial \underline{x}} \cdot \underline{(\bar{p})} + \beta (\langle u_i \rangle - \bar{v}_i) \langle \rho \rangle + \underline{\bar{\kappa}_i} \langle \rho \rangle$$

total pressure

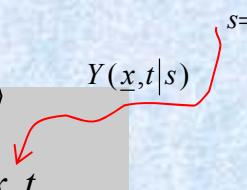
drag force

$$\text{Eqn of state } \frac{p_{ij}}{\langle \rho \rangle} = \bar{v}'_i \bar{v}'_j + \lambda_{ij}$$

Momentum equation as a diffusion equation

$$\langle \rho \rangle \bar{\underline{v}} = \langle \rho \rangle \underline{v}_C - \underline{\varepsilon} \cdot \frac{\partial \langle \rho \rangle}{\partial \underline{x}} - \beta^{-1} \langle \rho \rangle \frac{D \bar{\underline{v}}}{Dt} \quad \text{Momentum eqn.}$$

$$\underline{v}_C = \langle \underline{u} \rangle + \underline{v}_d \quad \underline{v}_d = -\beta^{-1} \frac{\partial}{\partial \underline{x}} \cdot \bar{\underline{v}' \underline{v}'} - \beta^{-1} \underline{\kappa} \quad \begin{array}{l} \text{Drift due spatial inhomogeneity} \\ \text{turbophoresis} \end{array}$$



$$\underline{\varepsilon} = \beta^{-1} \left(\bar{\underline{v}' \underline{v}'} + \underline{\lambda} \right) = \int_0^\infty \underbrace{\langle \underline{u}_p(0) \underline{u}_p(t) \rangle}_{\text{Lagrangian}} dt \quad \begin{array}{l} \text{Homogeneous stationary turbulence} \\ \text{Long time particle diffusion coefficient} \end{array}$$

Diffusion coefficient versus particle inertia

Homogeneous stationary turbulence

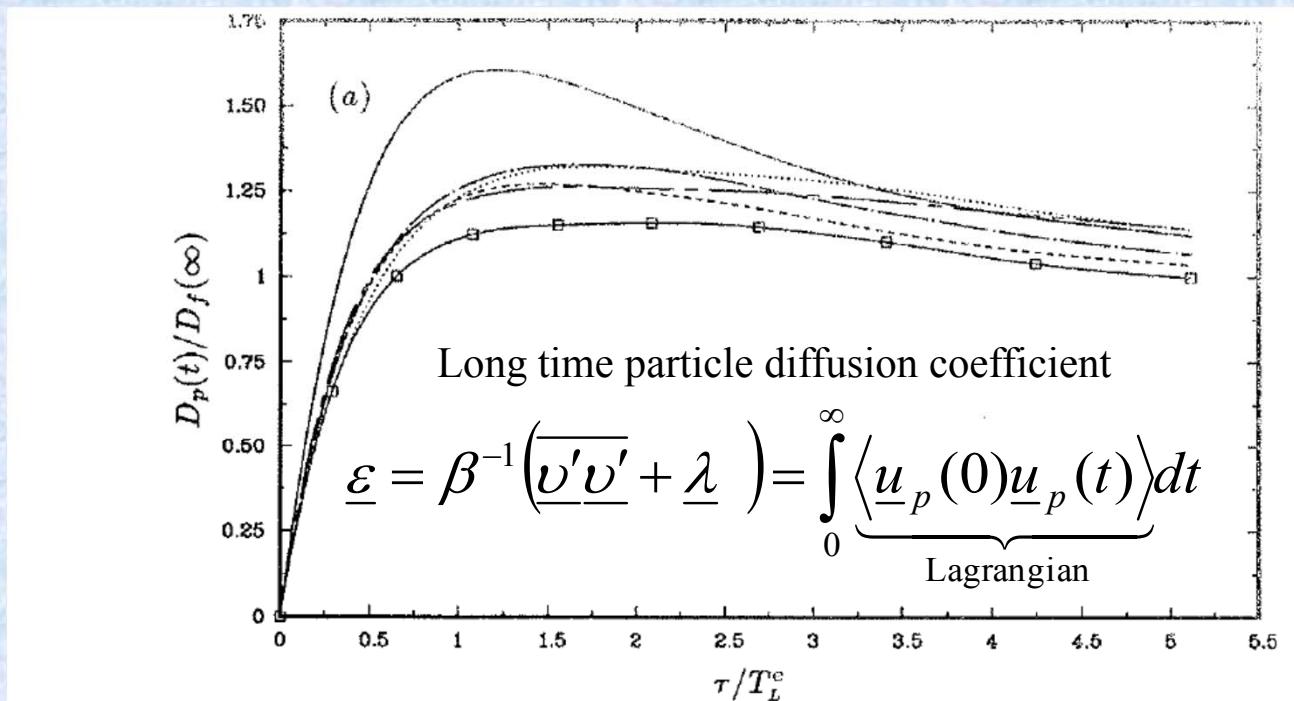


FIGURE 4.6A. Effect of inertia on particle eddy diffusivity, $Re_\lambda = 30.8$. $\square - \square$, fluid (Case DI1); $- - -$, $\tau_p/T_f = 0.05$; $- \cdots -$, $\tau_p/T_f = 0.11$; $\cdots \cdots$, $\tau_p/T_f = 0.33$; $- \cdots -$, $\tau_p/T_f = 0.65$; $- - -$, $\tau_p/T_f = 1.09$.

Particle kinetic stress transport equation

Kinetic stress flux

$$\langle \rho \rangle \frac{D}{Dt} \overline{v'_m v'_n} = -\frac{\partial}{\partial x_i} \langle \rho v'_i v'_m v'_n \rangle$$

Work done by total stresses

kinetic stresses

$$\overbrace{\langle \rho \rangle \overline{v'_n v'_i}} + \underbrace{\langle \rho \rangle \bar{\lambda}_{ni}}$$

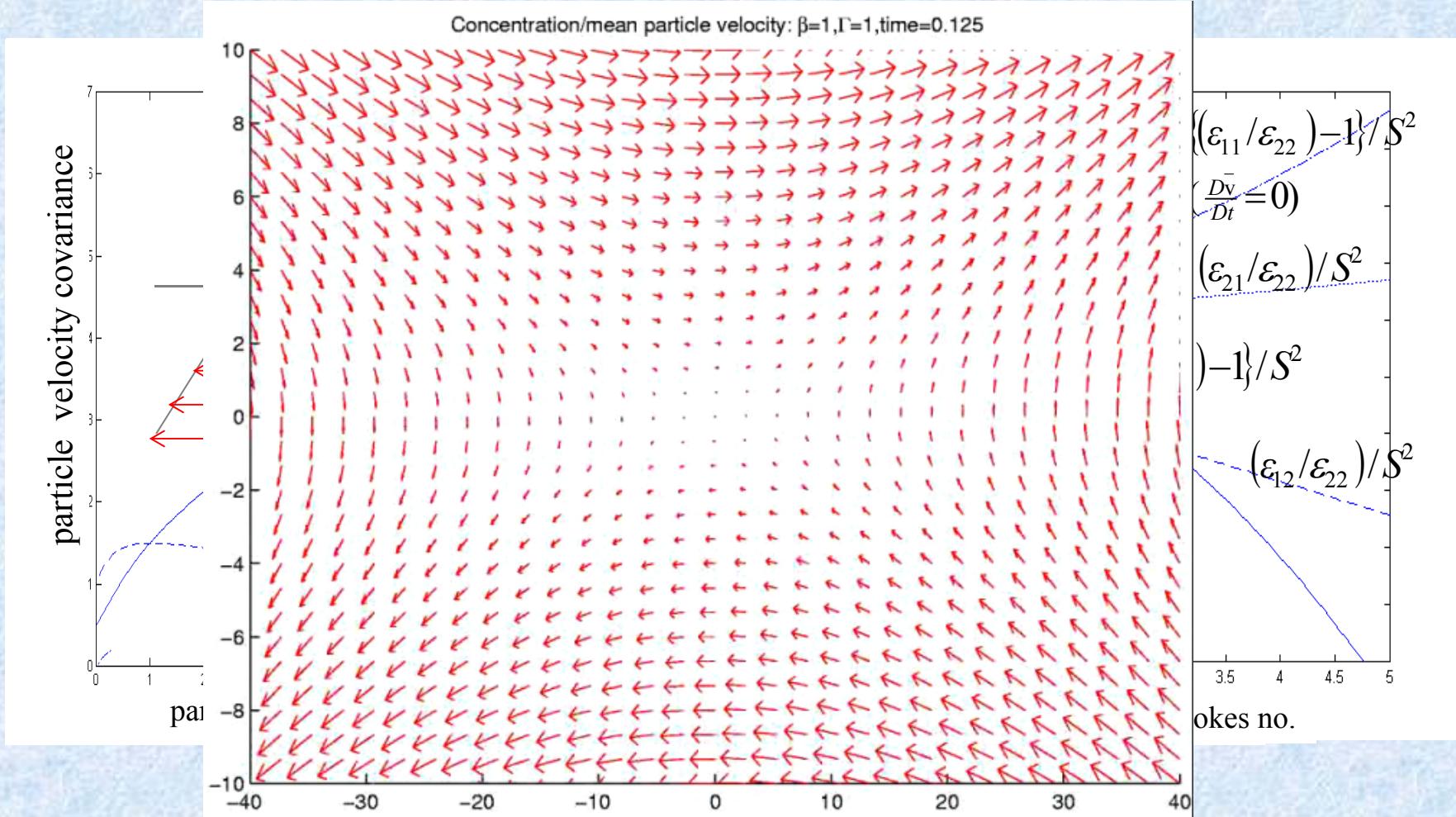
stresses from turbulent forces

$$-\left(p_{ni} \frac{\partial \overline{v_m}}{\partial x_i} + p_{mi} \frac{\partial \overline{v_n}}{\partial x_i} \right)$$

$$-2\beta \langle \rho \rangle \left(\overline{v'_m v'_n} - \overline{\mu_{mn}^S} \right) \rightarrow \frac{1}{2} \left[\overline{u'_m v'_n} + \overline{v'_m u'_n} \right]$$

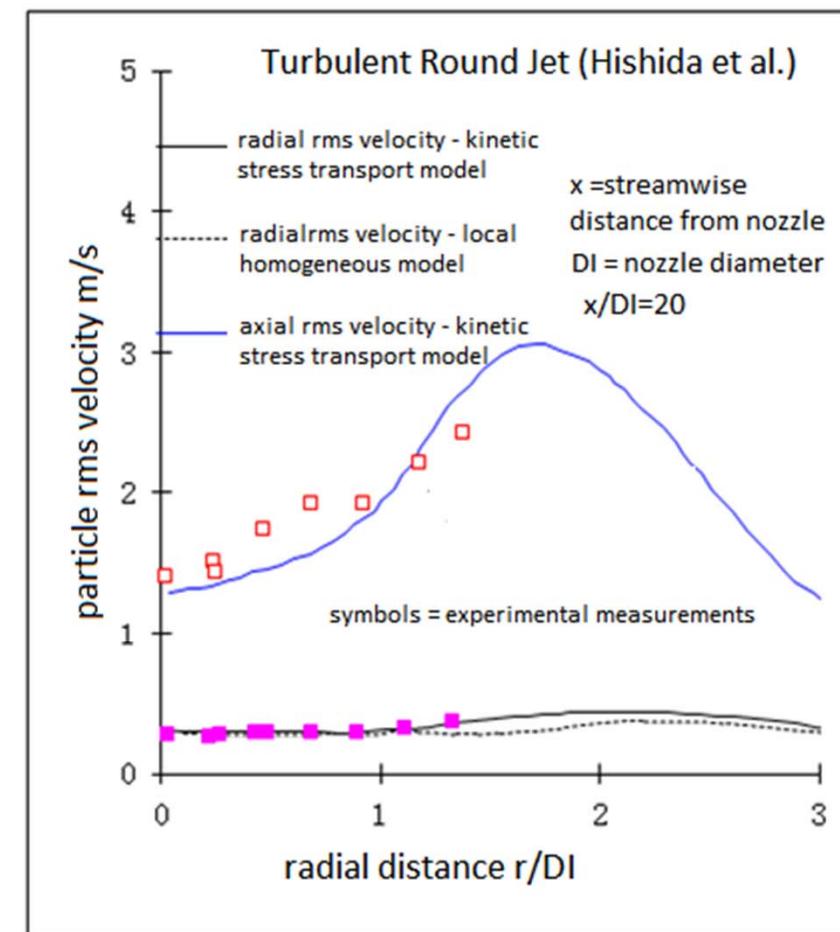
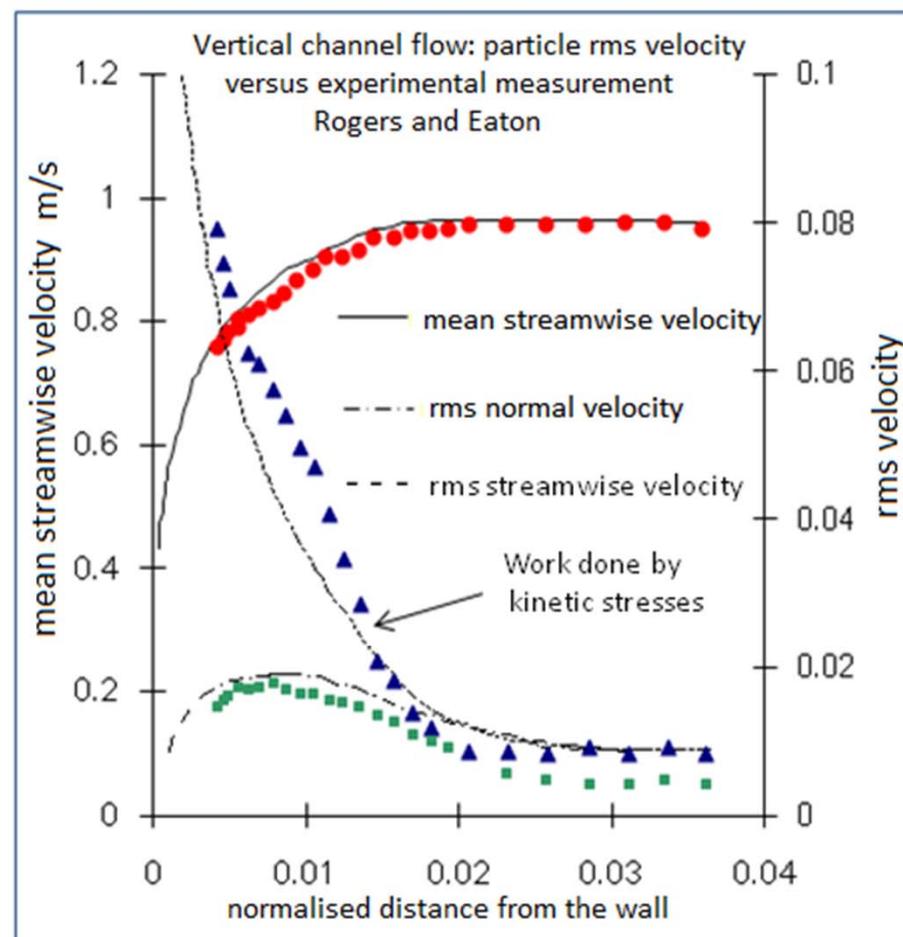
Particle-fluid
velocity covariances

Dispersion in a simple shear



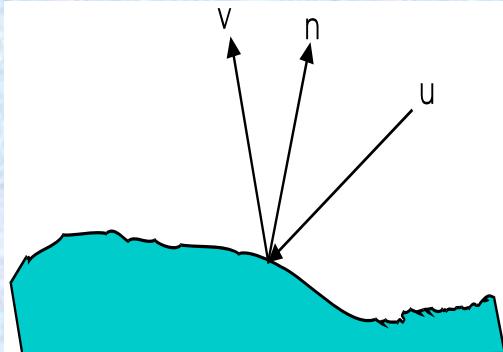
Predictions versus experimental measurements

Simonin et al.



Near-wall behaviour

- influence of particle wall interactions
 - scattering & absorption/deposition/ bounce /resuspension



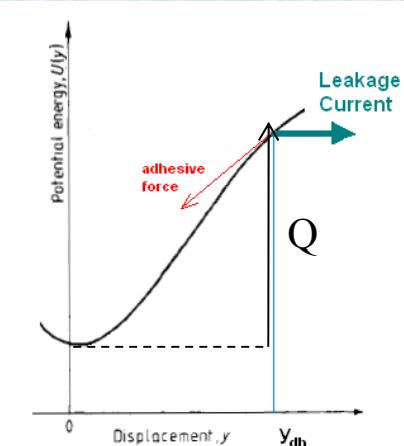
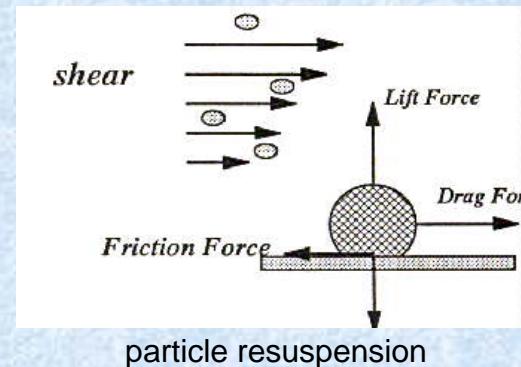
boundary conditions

$$y_p(\underline{g}, \underline{x}, t) = \int_{u \cdot n \leq 0} u P(u, \underline{x}, t) \Theta(v|u) du$$

$\Theta(v|u)$ = distribution of v given u

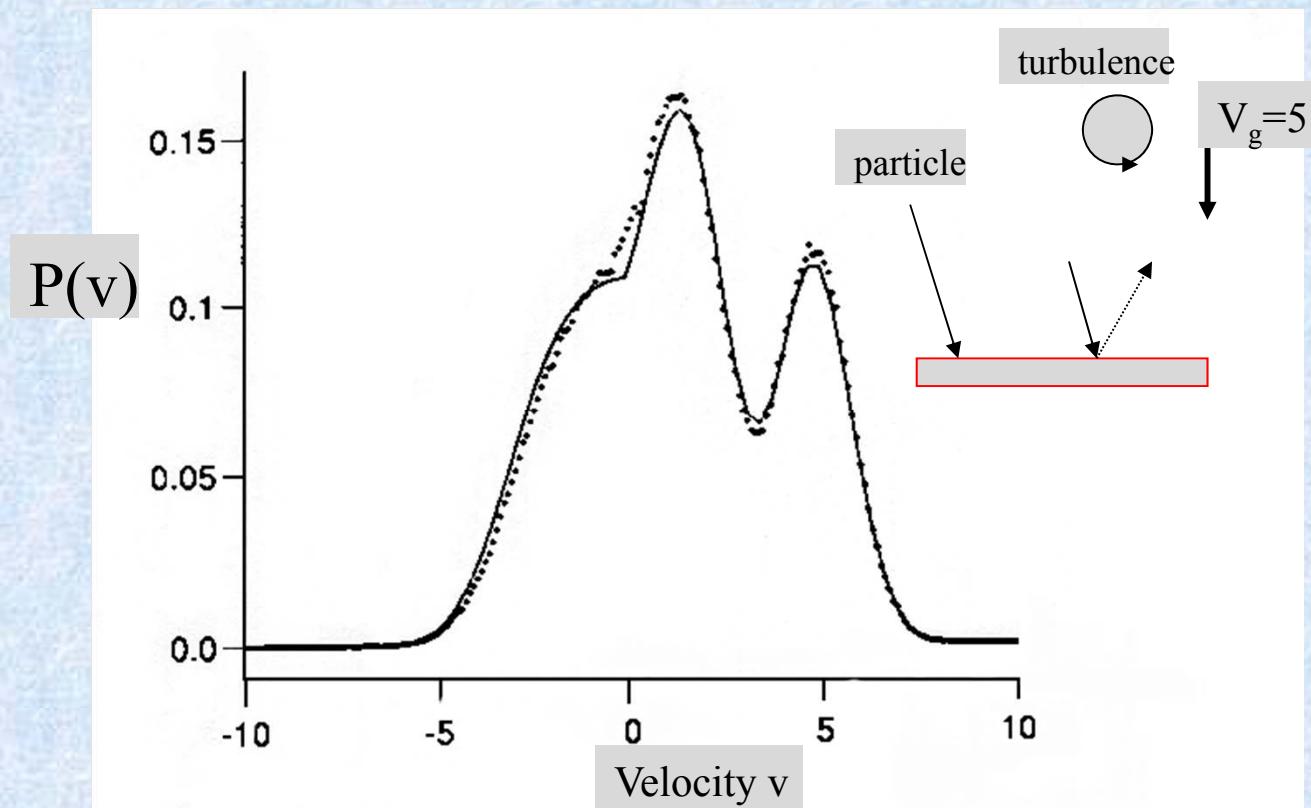
$$p = \omega \exp - Q / 2\langle PE \rangle$$

- p , the resuspension rate constant
- ω , the typical frequency of vibration,
- Q height of adhesive potential well,
- $\langle PE \rangle$ average potential energy of particle in the well.



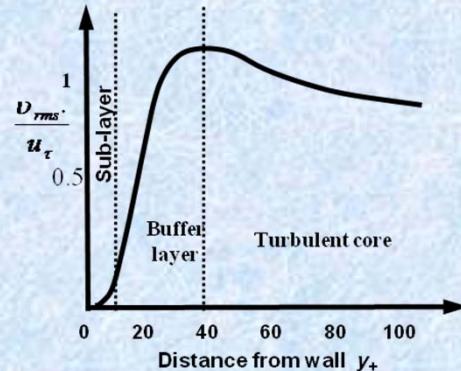
Particle escape from potential well

Particle wall impacts with absorption

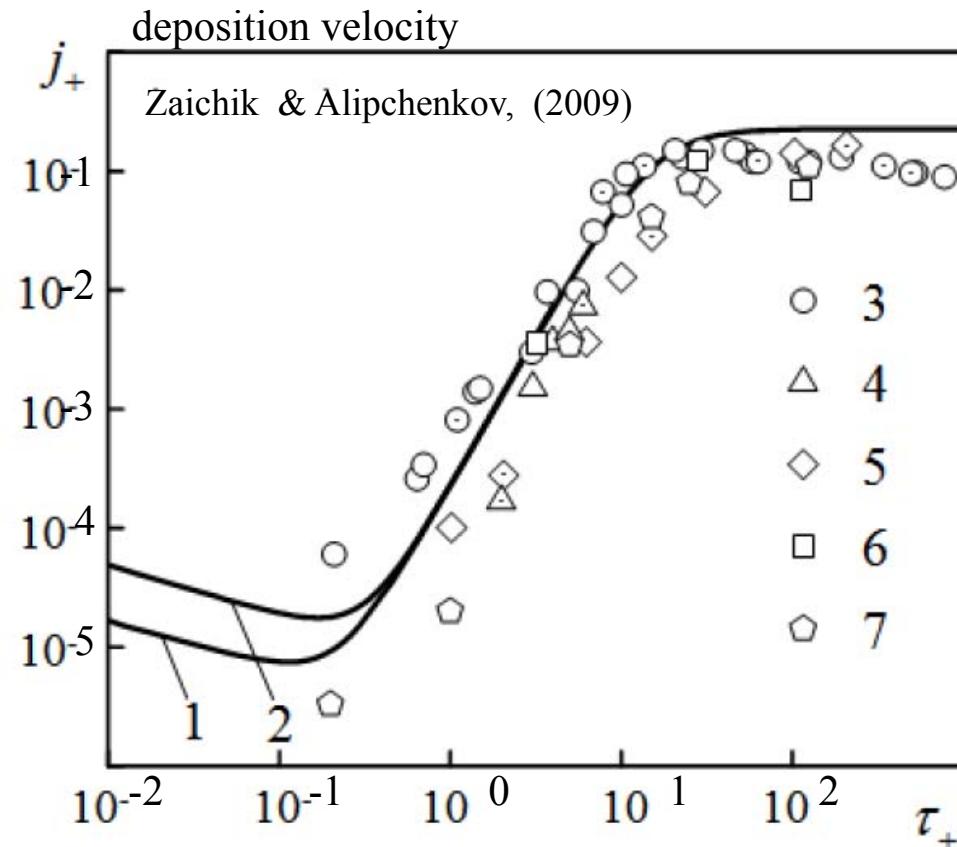


Critical impact velocity $v_c=5$, settling velocity $v_g=5$
(normalized on particle rms velocity for perfect reflection)

Deposition in turbulent boundary layer



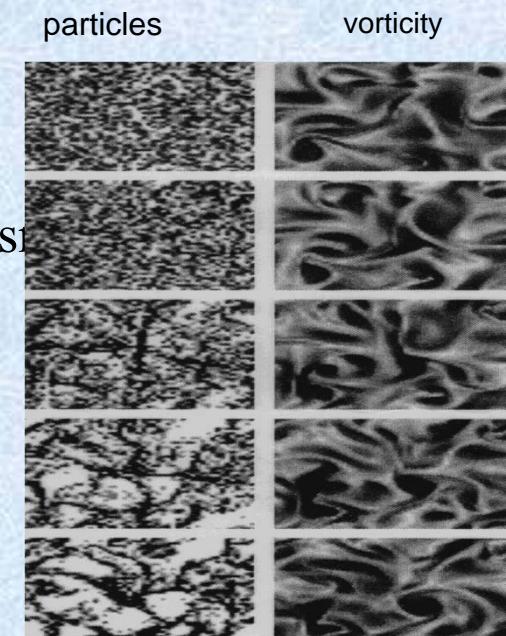
- rapid decay of turbulence near the wall
- particle not in local equilibrium with flow
- break down of gradient transport
- comparison of PDF results with experimental results



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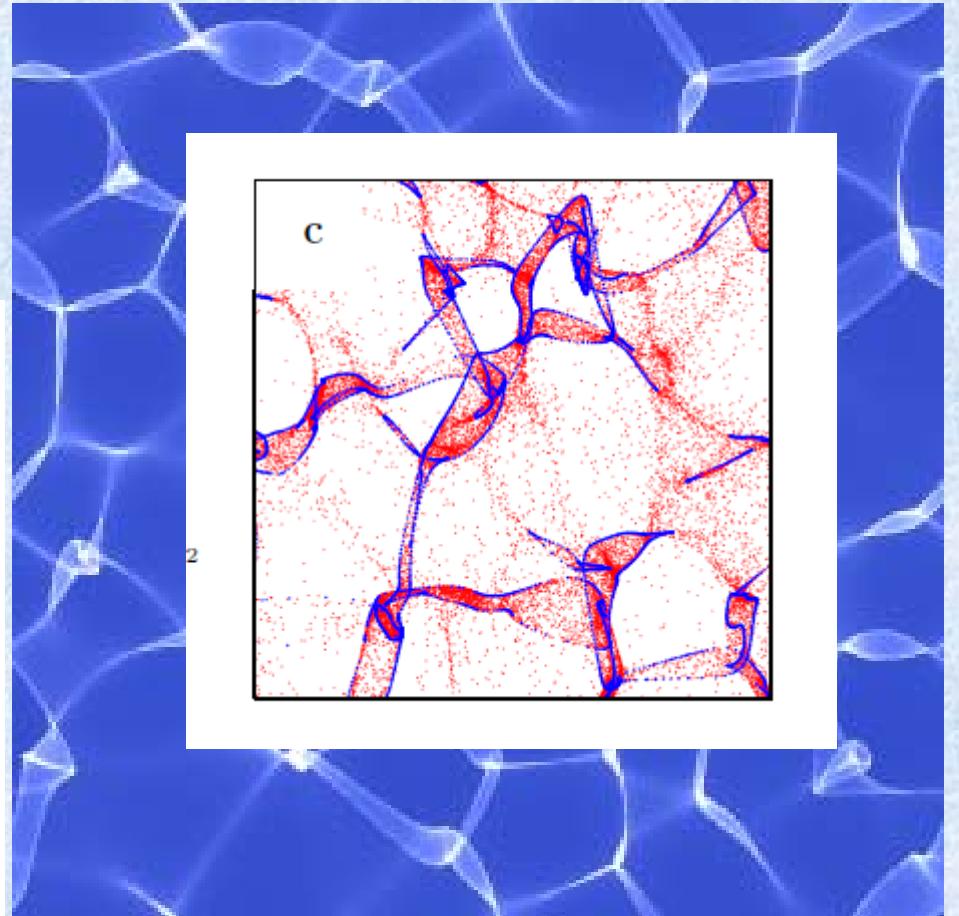
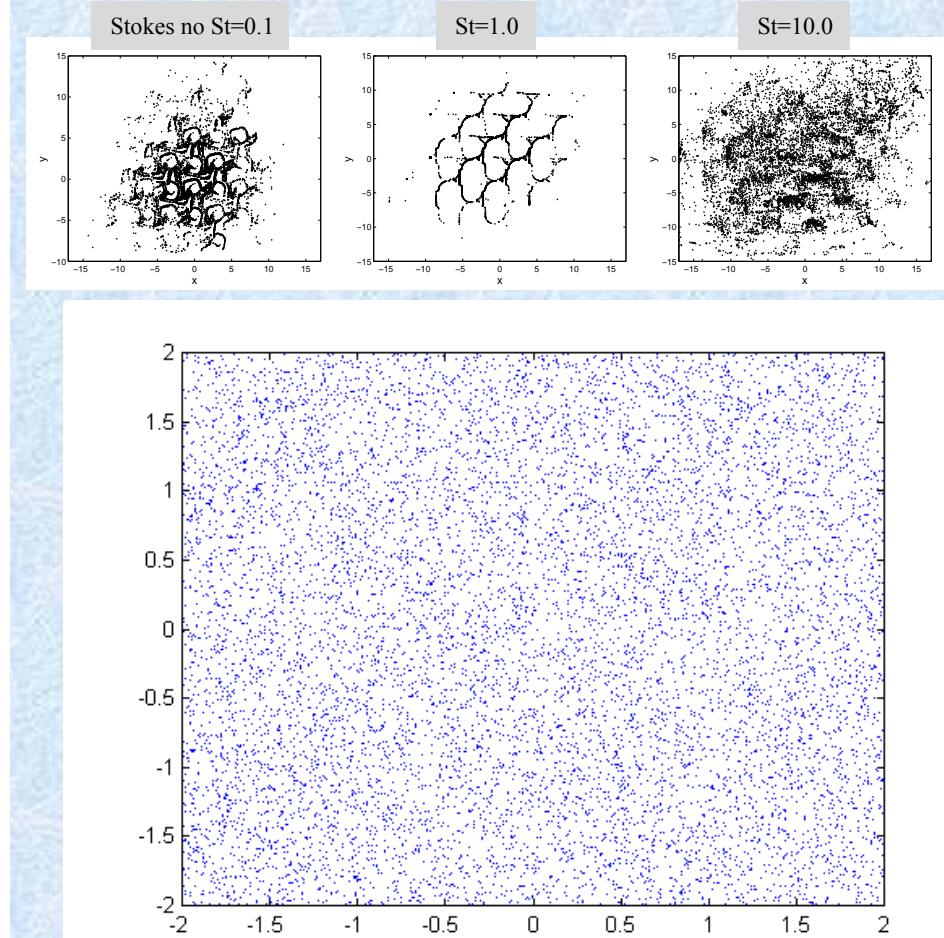
Two-particle dispersion

- Segregation/clustering
 - Full Lagrangian approach
 - Compressibility of a particle flow
 - Singularities in particle concentrations
- Random uncorrelated motion
- 2-particle PDF approach
 - Radial distribution
 - Collision kernel



Wang & Maxey JFM 1993

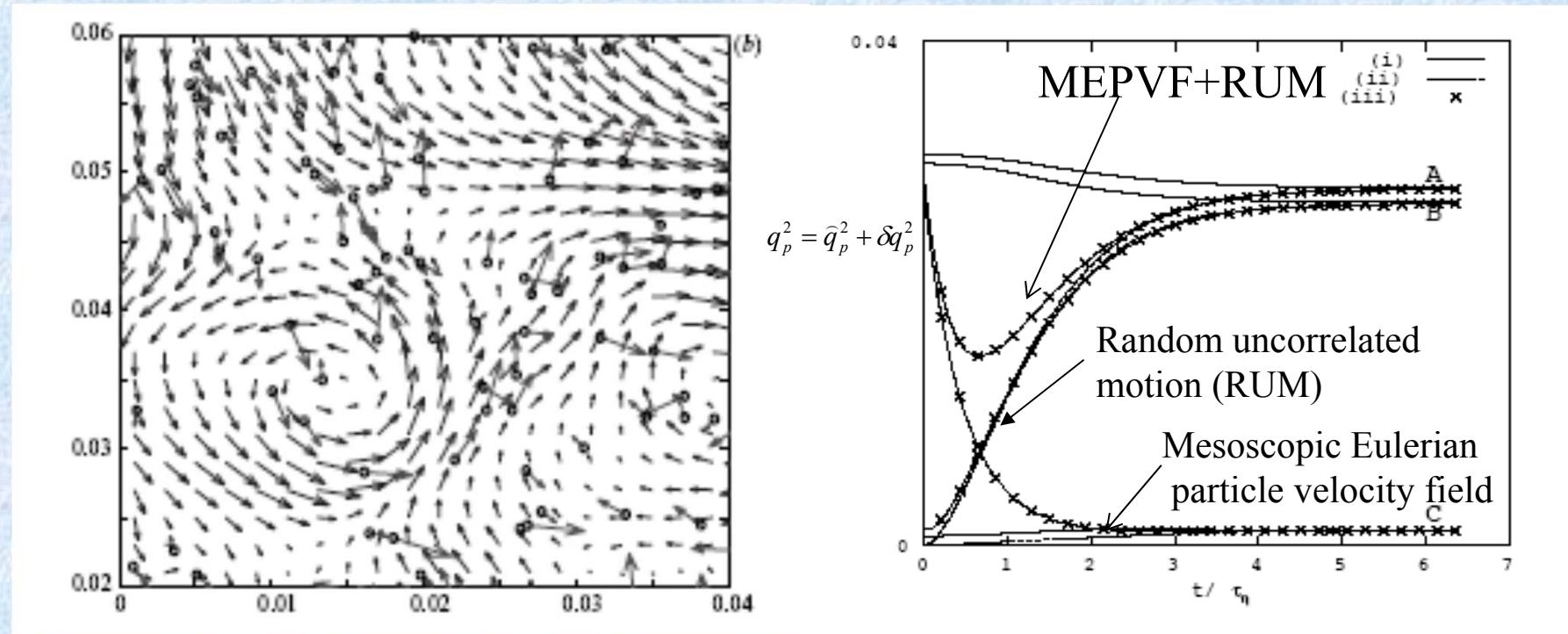
Unmixing by turbulent flows



Caustics (Wilkinson & Mehlig 2007)

Symposium Particle Transport, University of Aarhus 6-7 Nov, 2014

Random uncorrelated motion (RUM)

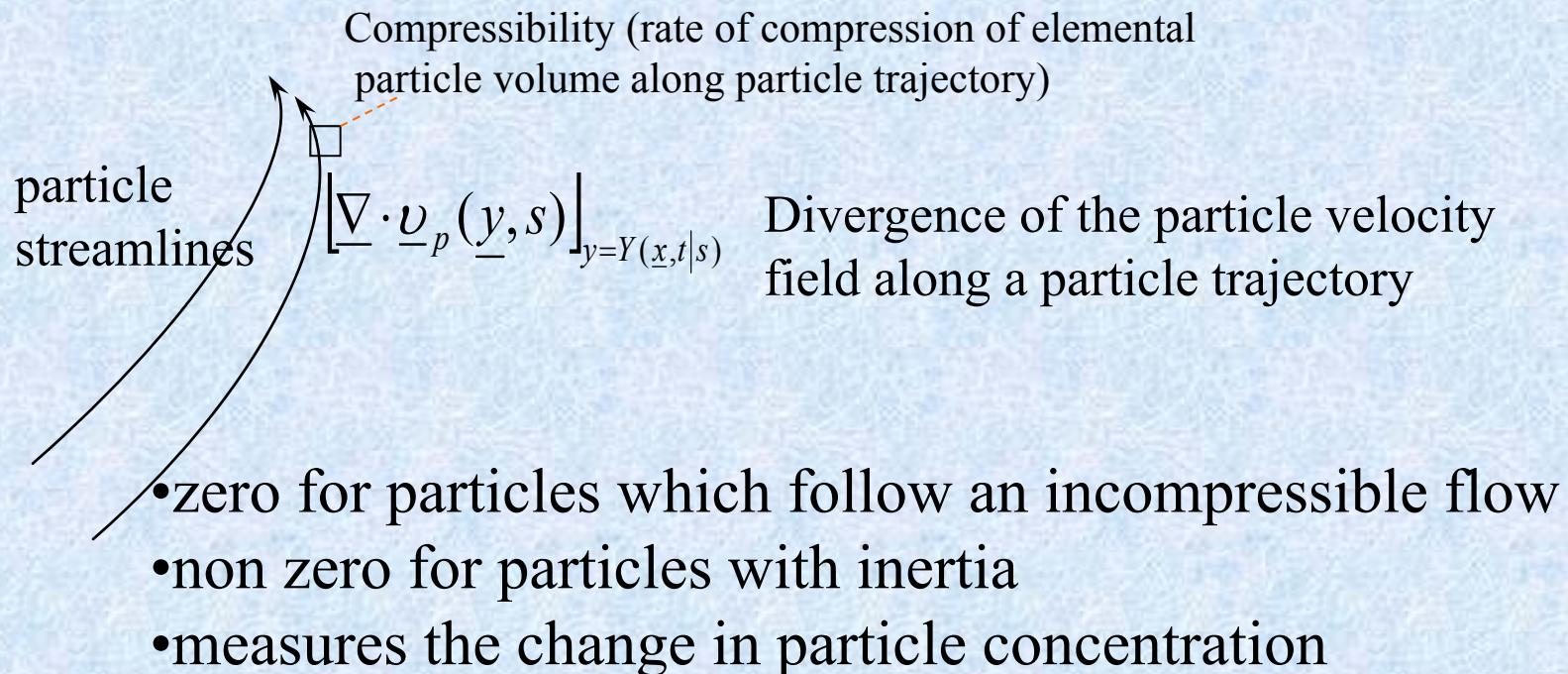


Février et. al JFM, 2005

$$\mathbf{v}_p^{(m)}(t) = \tilde{\mathbf{v}}_p(\mathbf{x}_p^{(m)}(t), t, H_f) + \delta\mathbf{v}_p^{(m)}(t).$$

Compressibility of a particle flow

Falkovich, Elperin, Wilkinson, Reeks



Measurement of the compressibility

Deformation
of elemental
volume

$$\rightarrow J_{ij} = \frac{\partial x_{p,i}(x_0, t)}{\partial x_{0,j}}; \quad J = |\det J_{ij}|$$

$\delta V(t)/\delta V(0)$ – volume fraction of
elemental volume of particles
along a particle trajectory

$$\text{compressibility } \nabla \cdot \underline{v}_p(x_0, t) = J^{-1} \frac{dJ}{dt} = \frac{d}{dt} \ln J \text{ compression}$$

can be obtained directly from solution of particle eqns. of motion

$(\underline{x}_p(t), \underline{v}_p(t), J_{ij}(t), J(t))$ - Full Lagrangian Method (FLM)

- Avoids calculating the compressibility via the particle velocity field
- Can determine the statistics of $\ln J(t)$ easily.

Particle trajectories in a periodic array of vortices

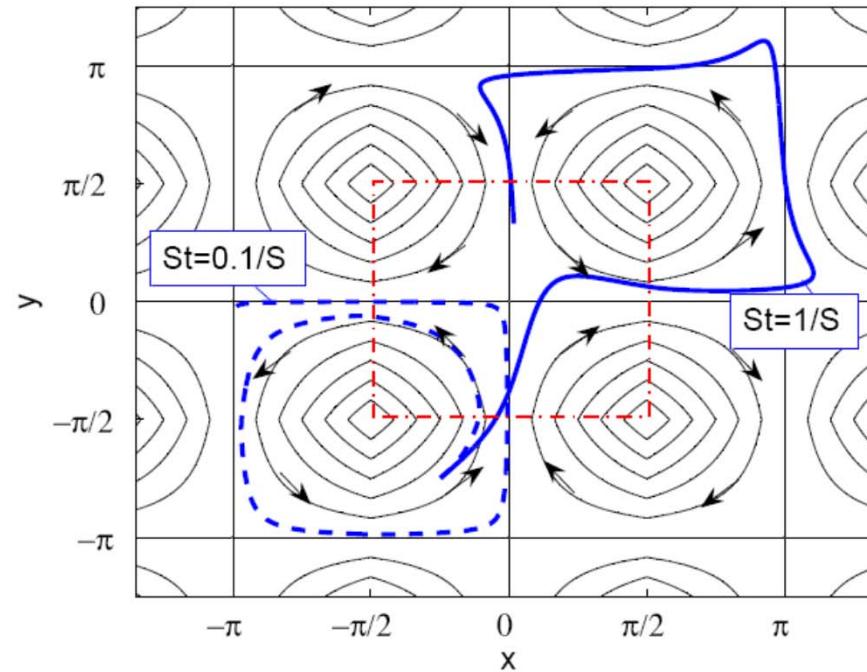


FIGURE 1. Particle trajectories in a frozen field of periodic vortices, for $St = 0.1/S$ (dashed blue line; heavily damped case) and $St = 1/S$ (solid blue line; lightly damped case), where S represents the strain rate in the flow. The two particles are released in $(x, y) = (-\pi/4, -3\pi/4)$ with a velocity equal to the local carrier flow velocity at time $t = 0$, and traced for a time $t = 20$. The highlighted area (red dash-dotted line) designates the basic element out of which the entire flow field is constructed.

Deformation Tensor \underline{J}

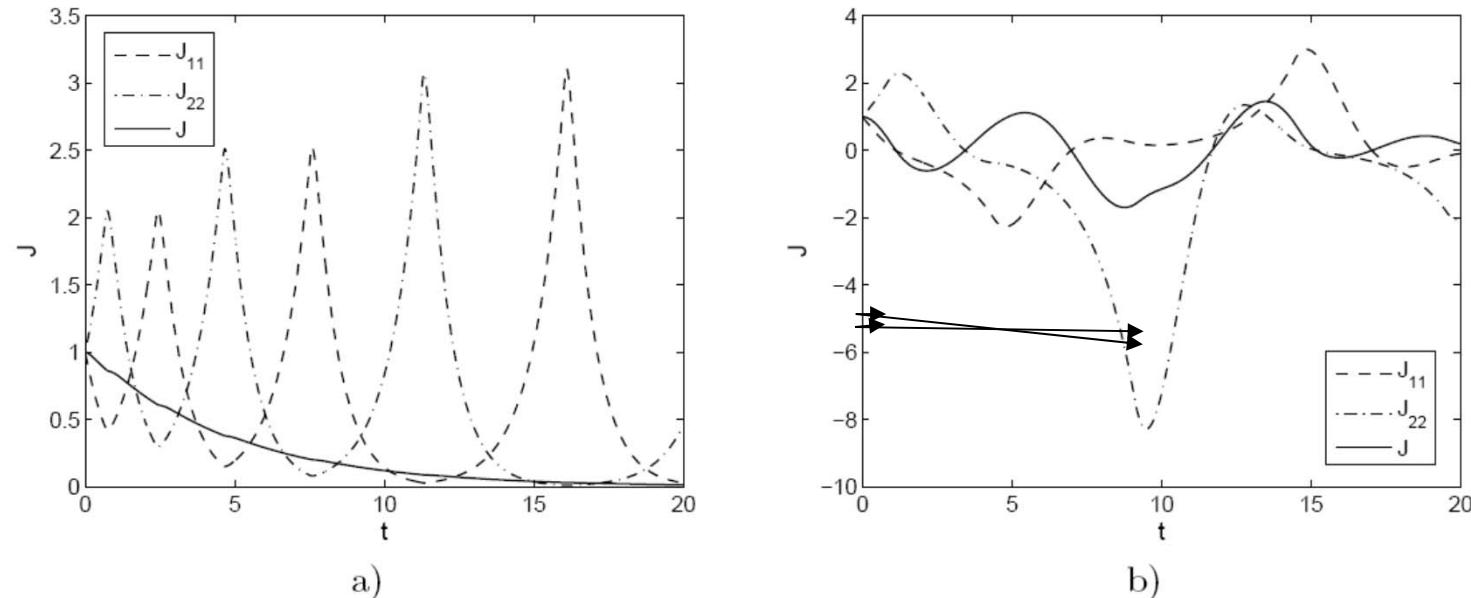
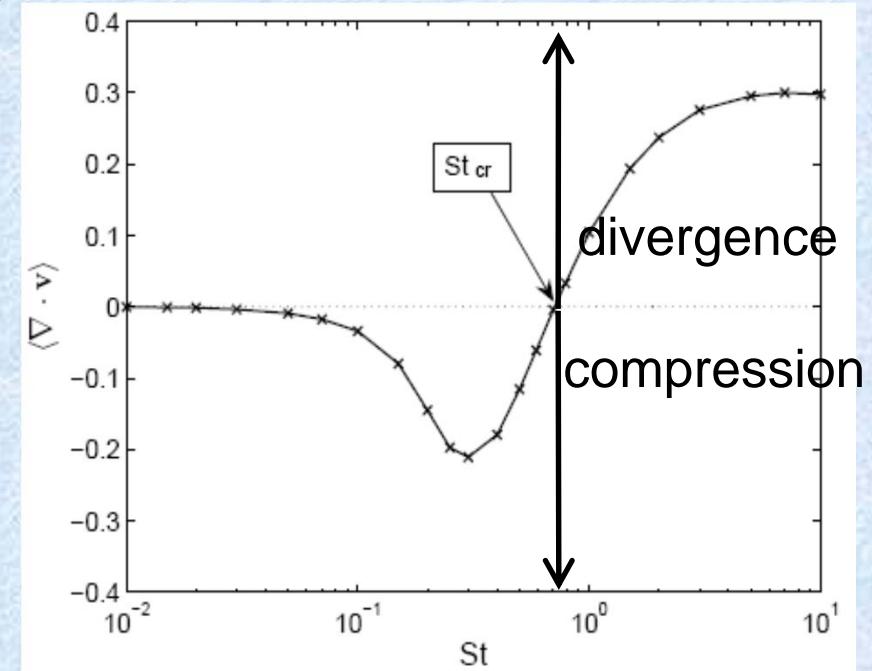
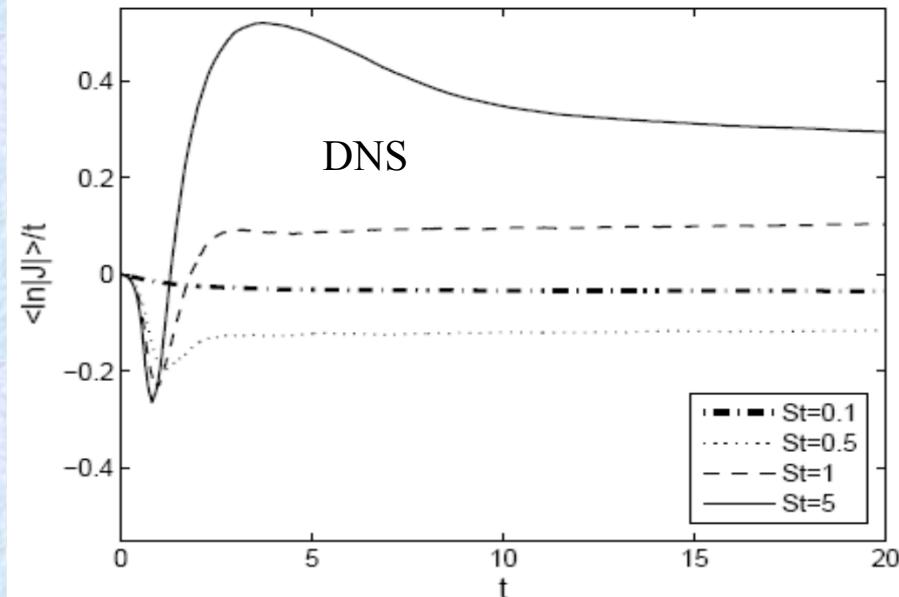


FIGURE 2. Values of the deformation J and the components of the deformation matrix J_{11} and J_{22} in the frozen field of periodic vortices depicted in Fig. 1, for (a) the heavily damped case $St = 0.1/S$, and (b) the lightly damped case $St = 1/S$. The values of J_{11} , J_{22} and J are calculated along the same two particle trajectories as plotted in Fig. 1. The strain rate is taken as $S = \sqrt{\overline{S^2}} = \sqrt{12}/\pi$.

Particle average compressibility

Compressibility of the pvf:

$$\frac{d}{dt} \langle \ln |J| \rangle = \langle \nabla \cdot \mathbf{v} \rangle$$

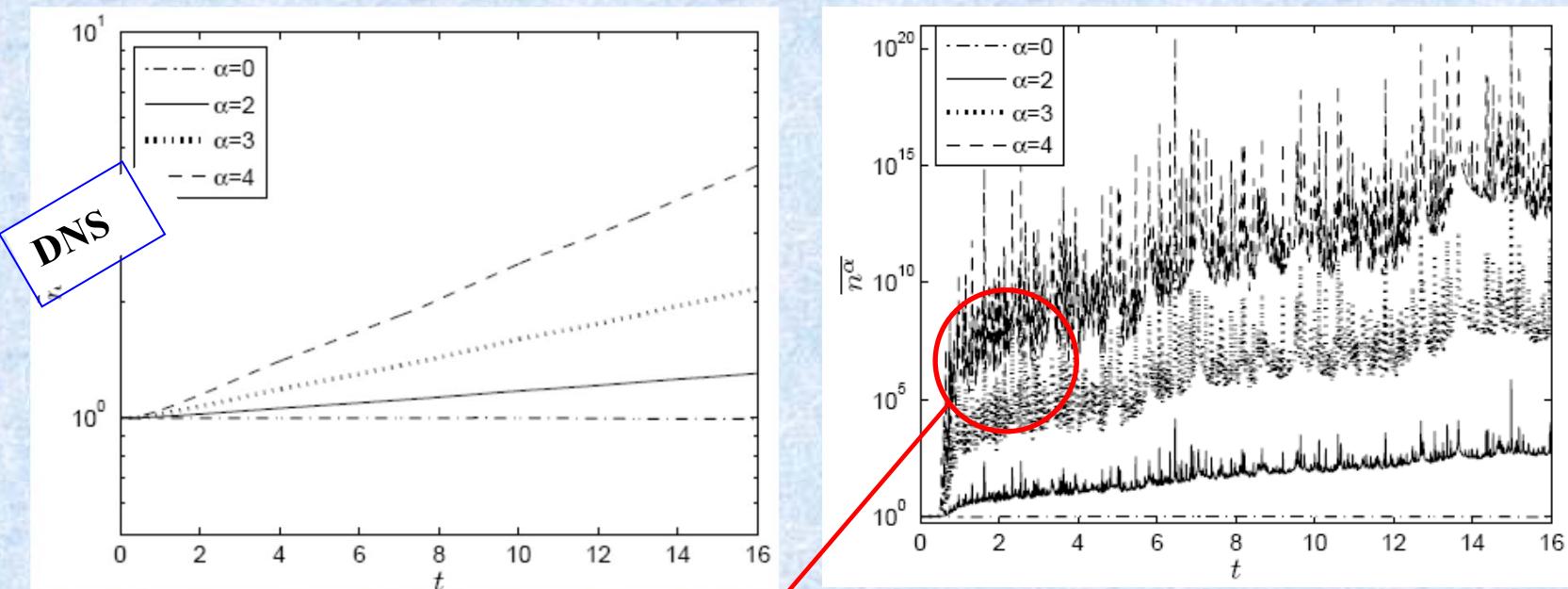


For a given flow field, there is a threshold St below which the segregation goes on indefinitely with time, and above which the dilation prevails over segregation.

Moments of particle number density

$$\begin{aligned} |J(t)| \approx n^{-1}(t) &\rightarrow n^\alpha \approx |J|^{-\alpha} \rightarrow \langle n^\alpha \rangle \approx \langle |J|^{-\alpha} \rangle \\ n^\alpha = \langle n^{\alpha-1} \rangle &= \langle |J|^{1-\alpha} \rangle \end{aligned}$$

St=0.1 **St=0.5**

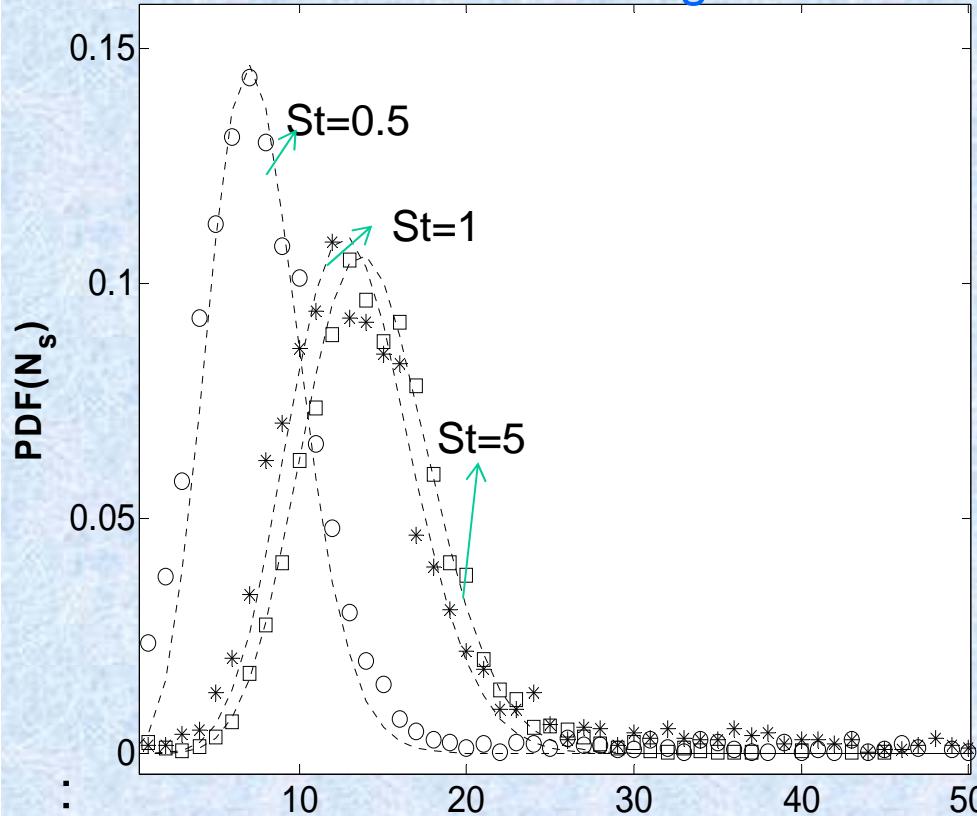


- Particle number density is spatially strongly intermittent
- The segregation goes on with time!
- The peaks reveal the presence of **singularities!**

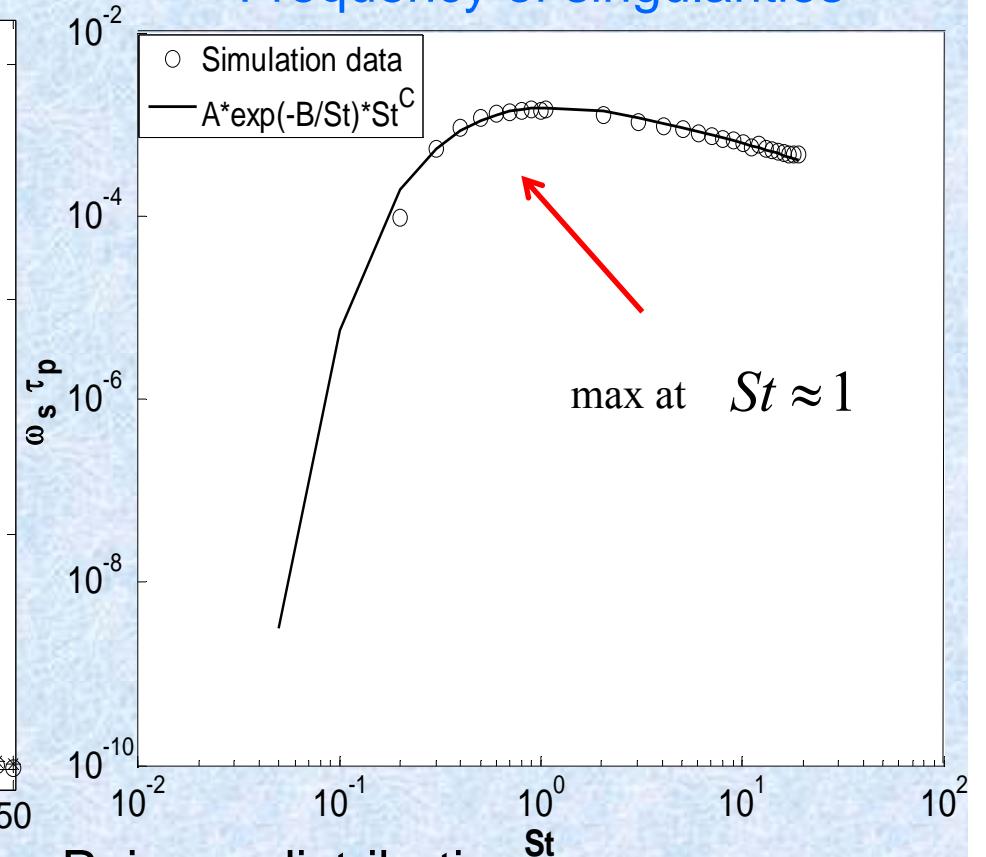
Singularities in the ptcl concentration field

Singularities correspond to $|J|=0$ events

Distribution of singularities



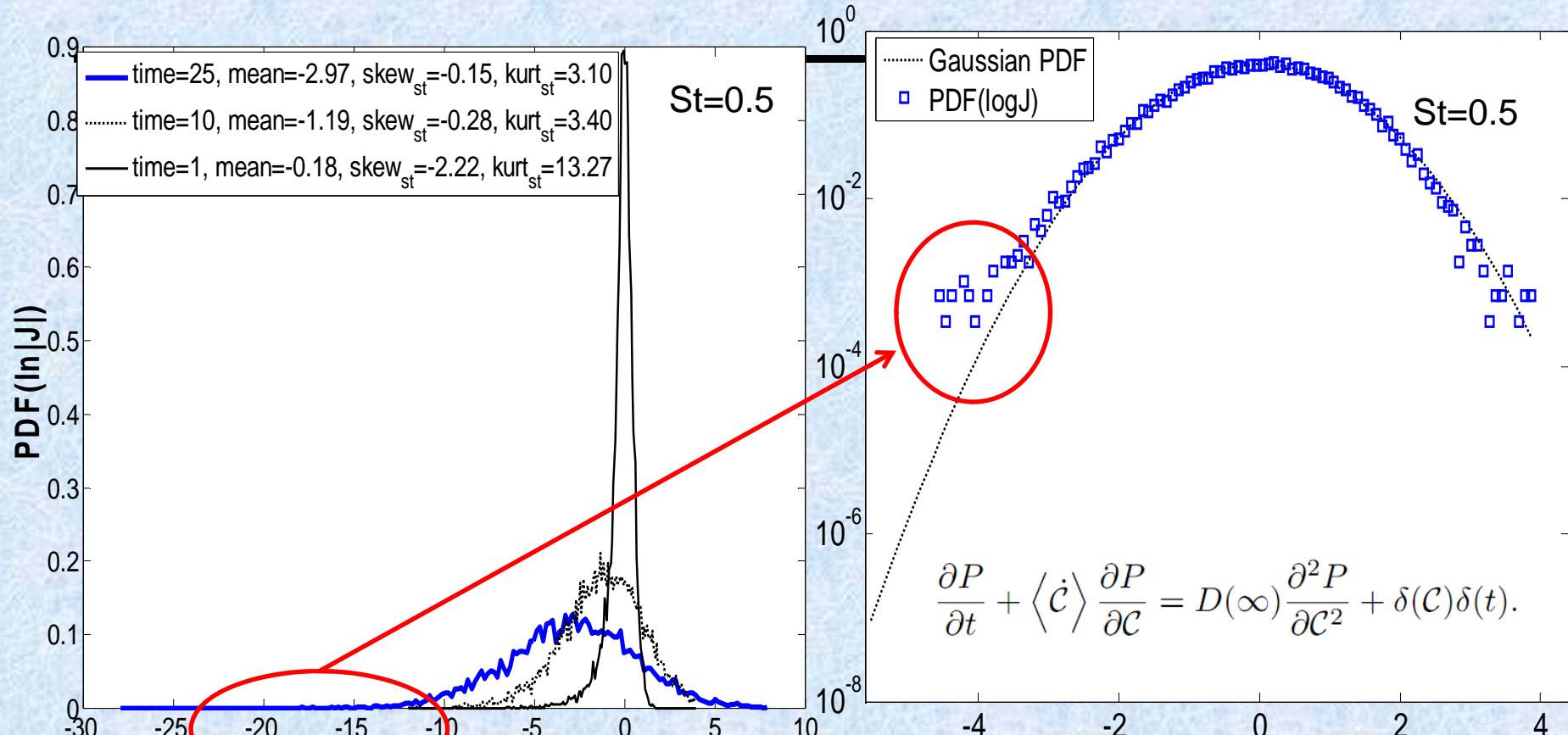
Frequency of singularities



The distribution of singularities follows a Poisson distribution

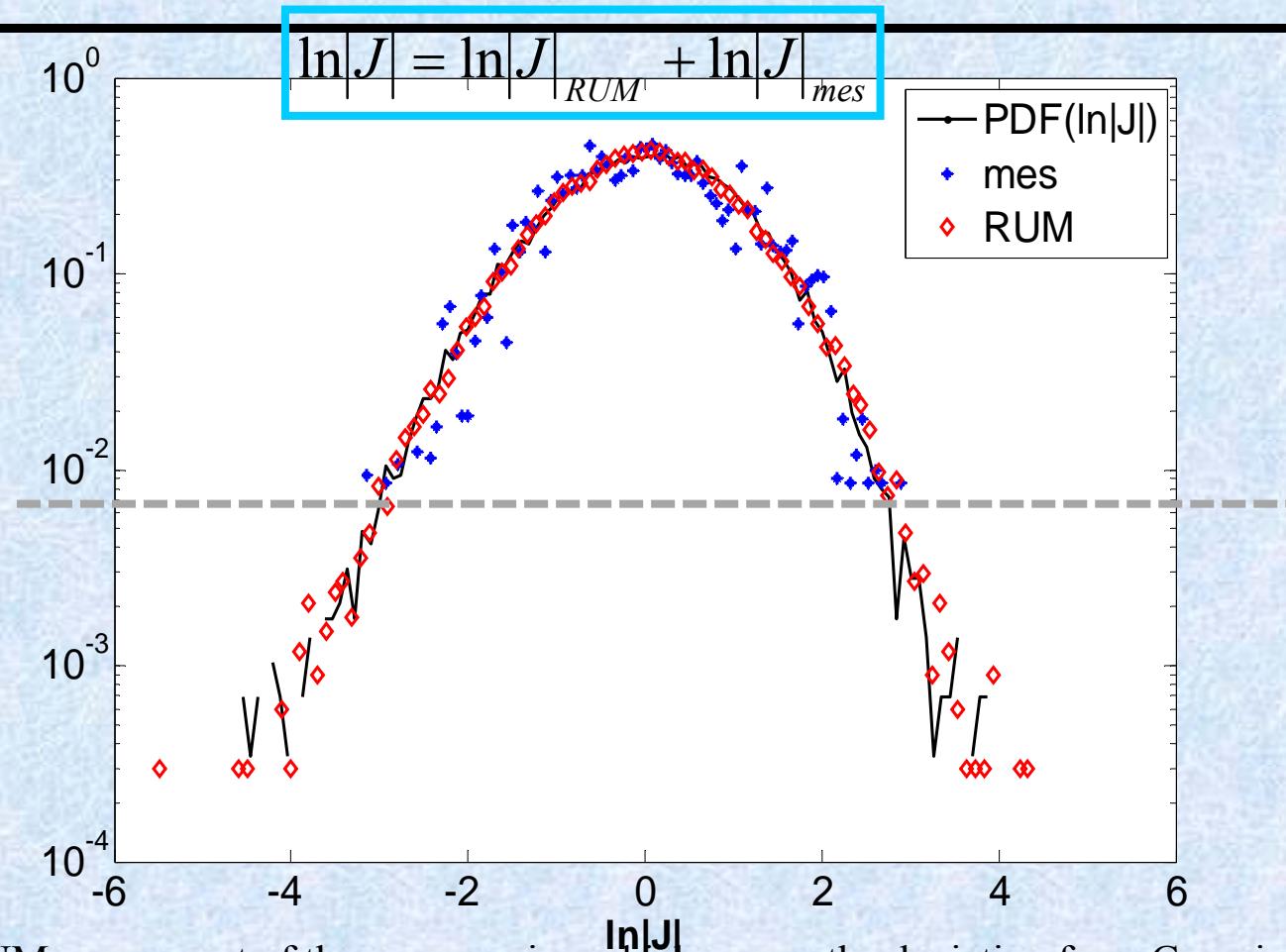
The maximum frequency of singularity events occurs for $St \approx 1$

Statistics of the compression $C=\ln|J|$



- The PDF of the compression looks Gaussian but..it is not!
- Singularities correspond to $\ln|J| \rightarrow -\infty$..what is the cause for the deviation from Gaussianity visible on the left tail of the curve?

The effect of RUM on $C = \ln|J|$



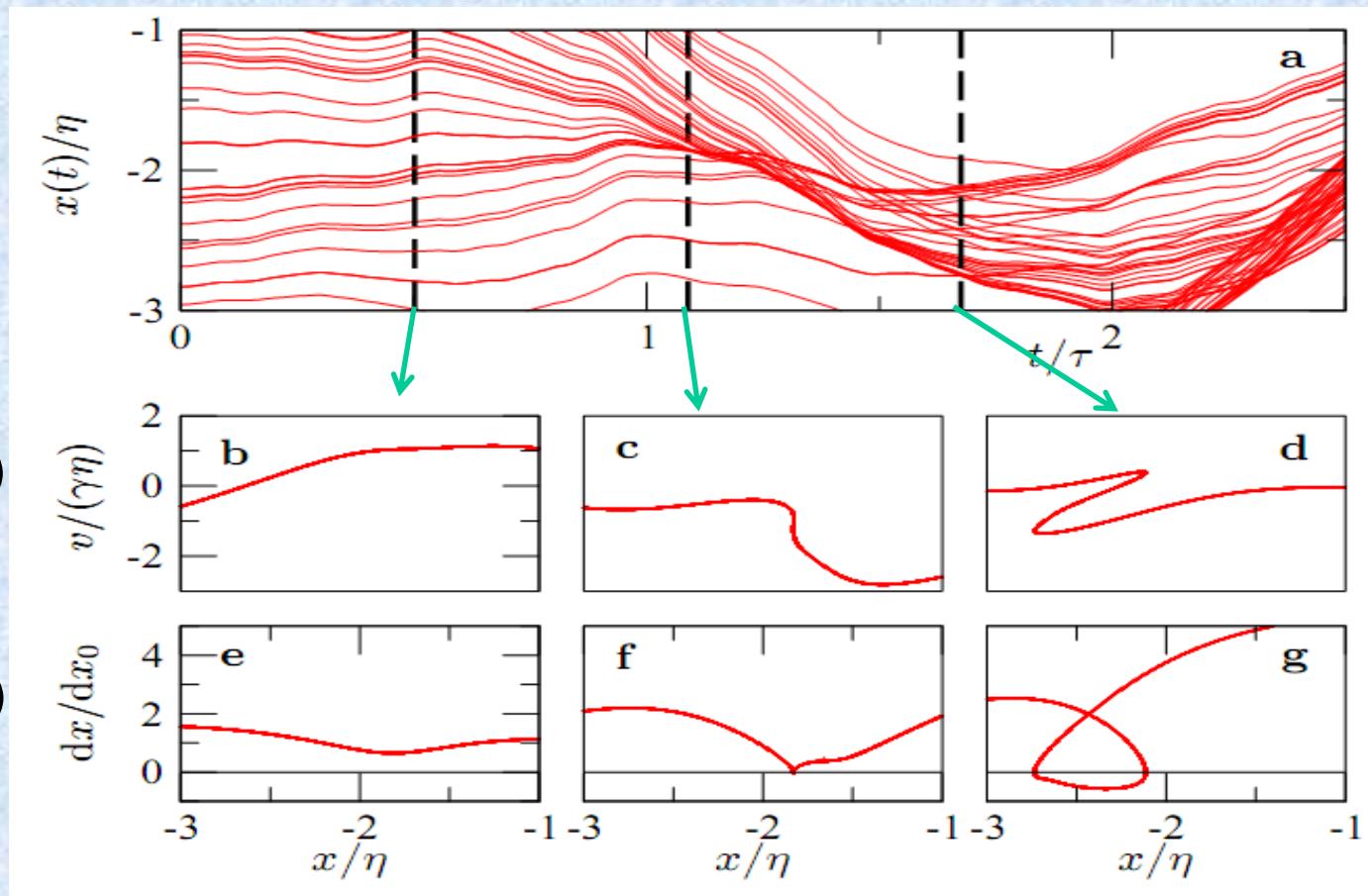
- It is the RUM component of the compression which causes the deviation from Gaussianity!
=>Singularities and RUM are intrinsically related

Singularities and RUM

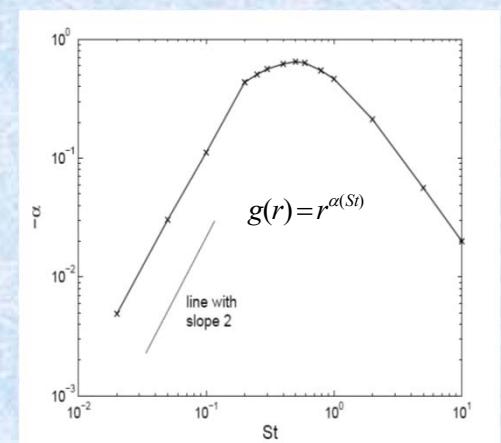
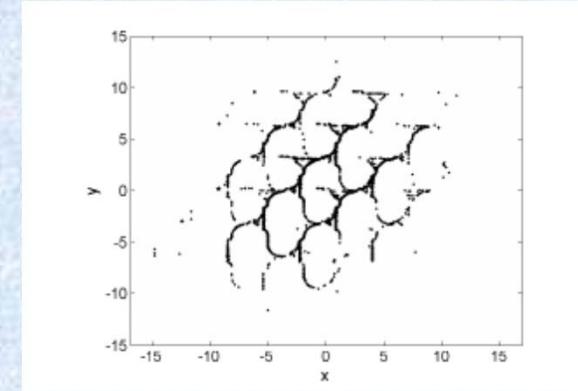
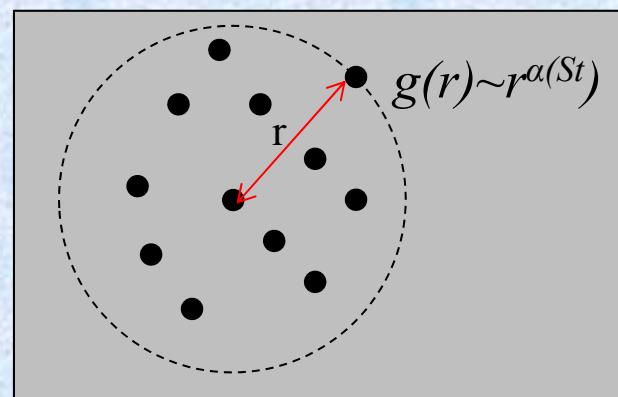
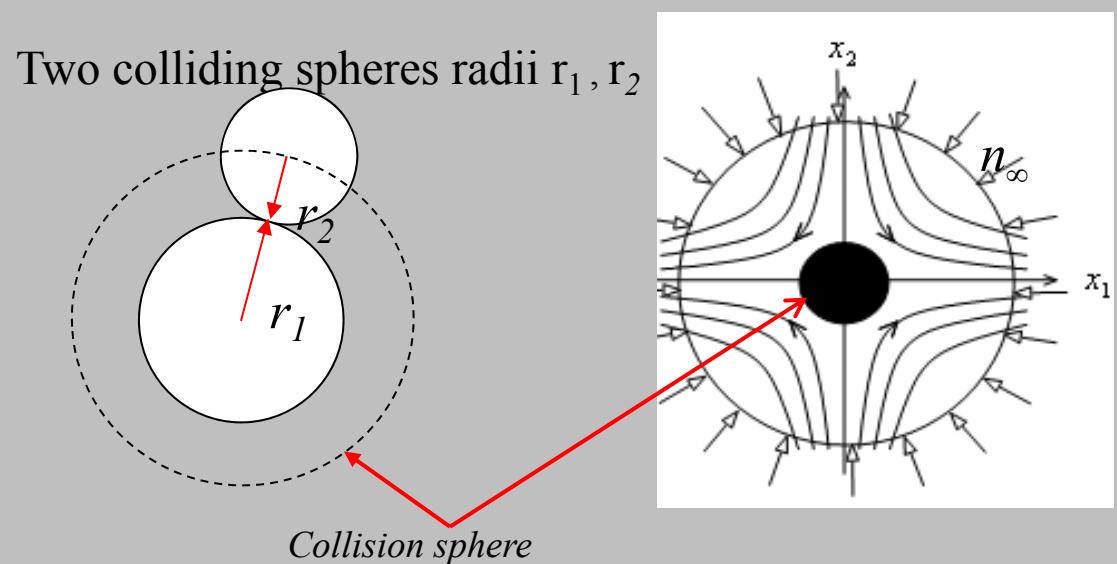
Trajectories

Velocity (RUM)

$|J|$ (singularities)



Pair dispersion and segregation



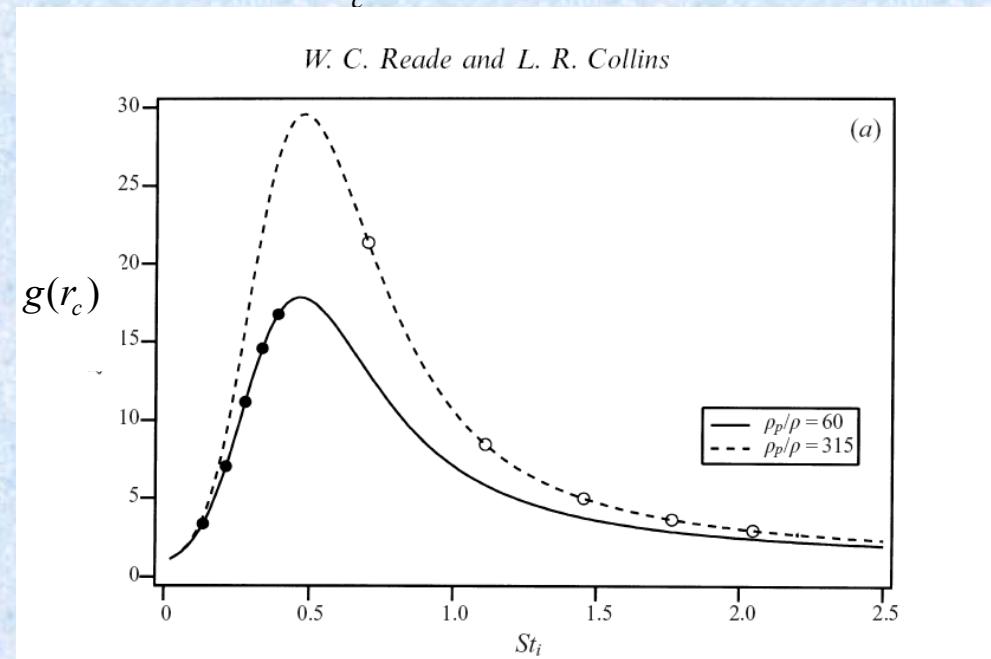
Agglomeration of inertial particles

Sundarim & Collins(1997) , Reade & Collins (2000): measurement of rdf's and impact velocities as a function of Stokes number St

$$K(r_1, r_2) = 4\pi r_c^2 g(r_c, St) \bar{w}_r(St)$$

RDF at r_c

Net relative velocity between colliding spheres along their line of centres



PDF Equation for relative dispersion

(Zaichik and Alipchenkov 2003,2009)

\underline{w} = relative velocity between identical particle pairs, distance \underline{r} apart

$\Delta \underline{u}(\underline{r},t)$ = relative velocity between 2 fluid pts, distance \underline{r} apart at time t

Structure functions $\langle \Delta u_r^2(r) \rangle, \langle \Delta u_\theta^2(r) \rangle \sim (r/\eta_K)^2$ $(r/\eta_K) \ll 1$

Eqns of Motion $\frac{d\underline{r}}{dt} = \underline{w} ; \frac{d\underline{w}}{dt} = \beta(\Delta \underline{u}(\underline{r},t) - \underline{w})$

$$\frac{\partial P}{\partial t} + \underline{w} \cdot \frac{\partial P}{\partial \underline{r}} - \beta \frac{\partial}{\partial \underline{w}} \cdot \underline{w} P(\underline{w}, \underline{r}, t) = - \frac{\partial}{\partial \underline{w}} \cdot \beta \bar{\Delta \underline{u} P}$$

↑ convection ↑

Net turbulent Force (diffusive)
 $\beta = St^{-1}$

mass $\frac{\partial \langle \rho \rangle}{\partial t} + \frac{\partial}{\partial x_i} \langle \rho \rangle \bar{w} = 0$ $\left(\frac{\partial}{\partial \underline{w}} \cdot \underline{\mu} + \frac{\partial}{\partial \underline{r}} \cdot \underline{\lambda} \right) P(\underline{w}, \underline{r}, t)$

momentum $\langle \rho \rangle \frac{D}{Dt} \bar{w}_i = - \frac{\partial}{\partial r_j} \langle \rho \rangle \bar{w}'_i \bar{w}'_j - \beta \bar{w}_i \langle \rho \rangle + \langle \rho \rangle \beta \bar{\Delta u}'_i$

————— $g(r) \approx r^{-\alpha_1 St^2}$ $St \ll 1$

PDF Equation predictions

Zaichik and Alipchenkov, NJP 2009

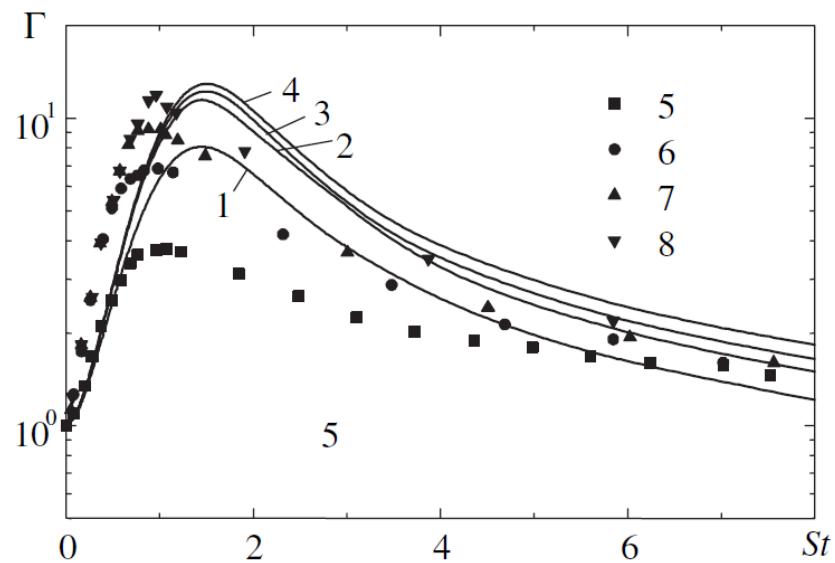


Figure 8. Influence of particle inertia on the RDF for $\bar{r} = 1$: 1–4, predictions; 5–8, DNS [8]; 1, 5, $Re_\lambda = 24$; 2, 6, $Re_\lambda = 45$; 3, 7, $Re_\lambda = 58$; 4, 8, $Re_\lambda = 75$.

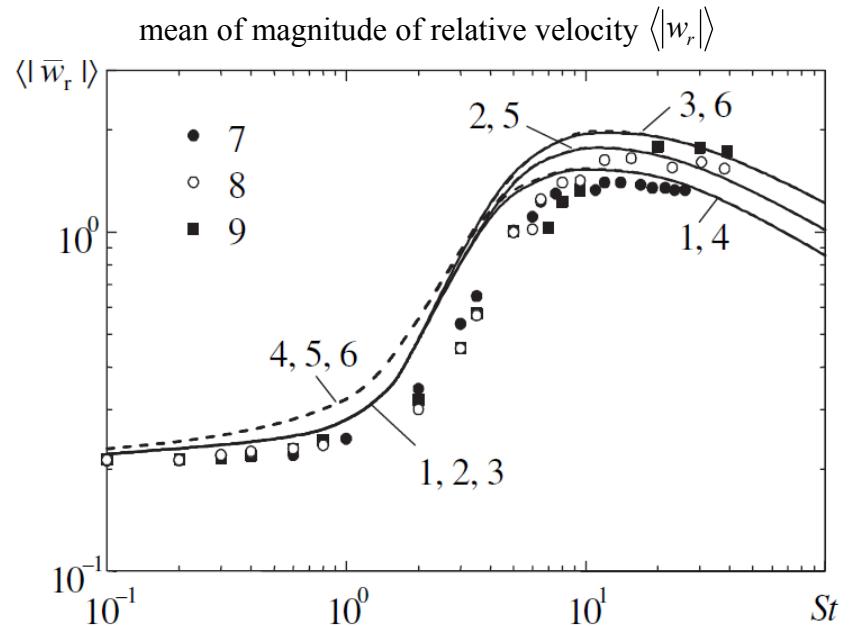
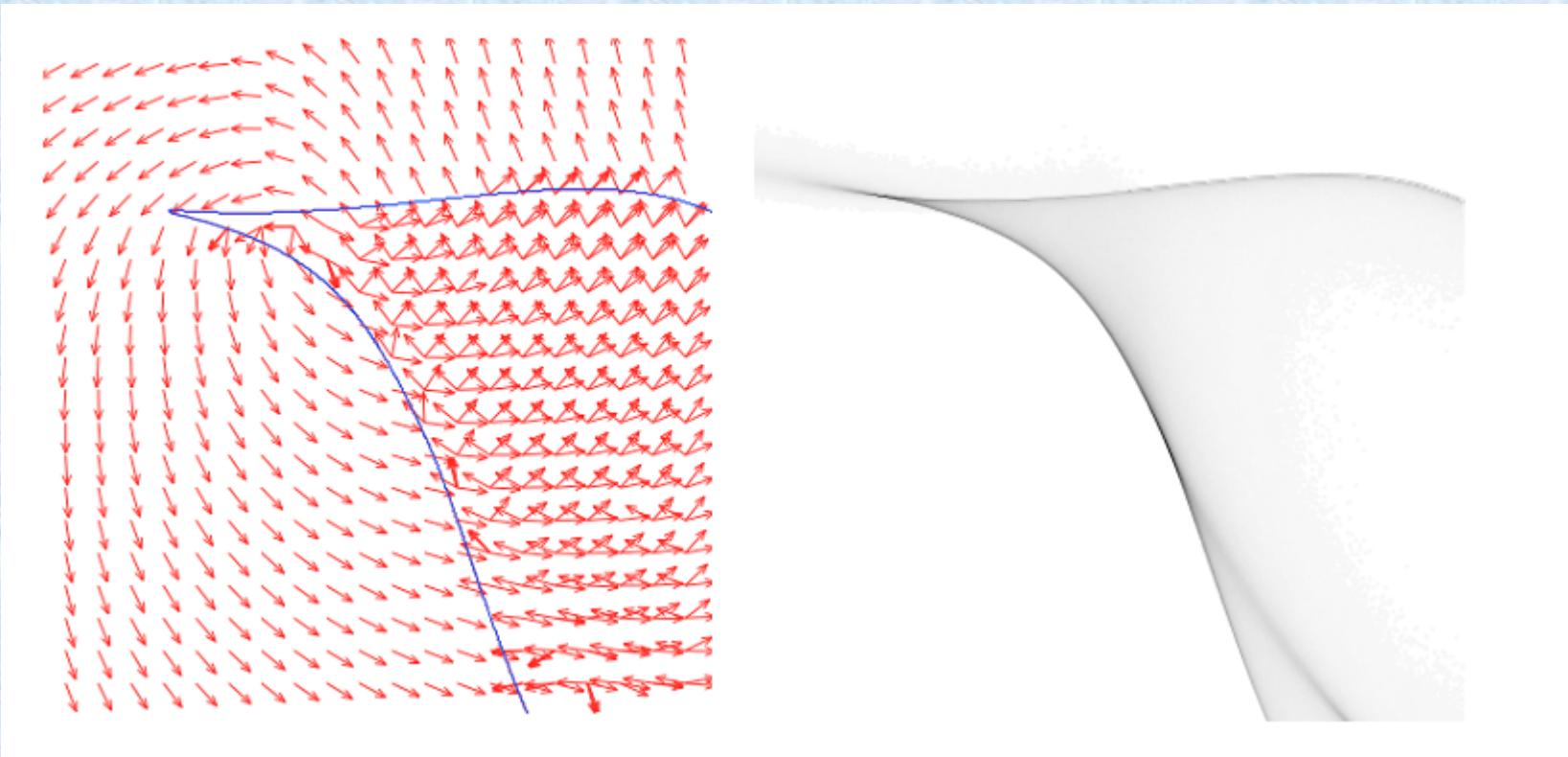


Figure 5. Influence of particle inertia on the mean relative velocity magnitude for $\bar{r} = 1$: 1–3, predictions with $\bar{d} = 0$; 4–6, predictions with $\bar{d} = 1$; 7–9, DNS [8]; 1, 4, 7, $Re_\lambda = 45$; 2, 5, 8, $Re_\lambda = 58$; 3, 6, 9, $Re_\lambda = 75$.

Caustics



Multivalued particle velocities in a
2-D random flow

Particle density

Summary & conclusions

- Transport of inertial particles turbulent flows
 - Methods and approaches
 - PDF approach / FLM
 - One particle dispersion
 - homogeneous and simple shear flows
 - inhomogeneous – turbulent boundary layer
 - Two particle dispersion
 - Unmixing of particle flows
 - compressibility of a particle flow
 - Singularities /intermittency
 - Formation of caustics

THANKS FOR YOUR ATTENTION

Any questions?